CASE STUDY

Red Oaks Latimer, Oklahoma

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RED OAKS, LATIMER, OKLAHOMA

1. SITE INFORMATION

1.1 Contacts

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1.2 Name, Location, and Description

The project site was the abandoned Bache and Denman underground coal mine acid mine discharge (AMD). Mining operations occurred from approximately 1907 to at least 1925. The mine is located in the Interior Province, Western Region Coal Field, in the Howe-Wilburton Coal District (Figure 1-1). The slope mine occupied approximately 47 acres and was mined using room-and-pillar methods. Since the stoppage of mining operations and the abandonment of the mine, AMD began to flow artesian through what is apparently a remnant sump room discharge pipe. AMD stripped approximately 1 acre of pasture land as the water flowed downgradient to Oak Ridge Creek, a primary, intermittent stream. Oak Ridge Creek is a tributary to Red Oak Creek, a seasonally interrupted third-order stream which flows to the Fourche Maline.

2. REMEDIAL ACTION AND TECHNOLOGIES

2.1 Passive Treatment Systems

This section contains text taken directly from "Design and Monitoring of a Mine Drainage Passive Treatment System Red Oak, OK," Robert W. Nairn, Ph.D., 2004.

Scope designs were developed based on available water quality and quantity data, established contaminant mass retention rates, and project-specific parameters (e.g., available land area, elevation changes, etc.). A five-cell passive treatment system was proposed, designed, and implemented, consisting of an initial oxidation pond and two sets of alternating vertical-flow and surface-flow cells. Flow through the system was designed to be completely dependent on hydraulic head differences. The system was designed to require limited maintenance and operation.

The initial oxidation pond was sized for iron removal from net alkaline mine drainage (the presumed case after CCP injection). The actual cell had approximate nominal depth of 5 ft, 2:1 inside slopes, 3:1 outside slopes, and a total surface area of 0.21 acres. This cell remained unplanted and contained native substrate with no additional material.



Figure 1-1. Red Oaks alkaline injection technology/passive treatment system, Red Oaks, Oklahoma. Latitude N $34^{\circ}55'59.4"$ (34.933167), longitude W $95^{\circ}2'5.6"$ (-95.064889); SE1/4, Section 1, Township 5N, Range 21E, Latimer County, OK.) Created with ArcGIS Desktop Version: 9.3.1

The vertical-flow cell design was based on designs successfully implemented at other locations. These cells were designed to both generate alkalinity and sequester metal contaminants. Each vertical-flow cell included three vertical sections. Layer 1 (standing water) provided water head necessary to drive water through the underlying substrate. A maximum of 3-ft vertical elevation (water depth) was provided, plus an additional 1 ft of freeboard. Layer 2 was designed to generate alkalinity via biotic and abiotic means. This section consisted of an approximately 3-ft-thick mixture of organic substrate (i.e., aged horse manure) and high-quality limestone in an approximately 2:1 ratio by volume. Layer 3 was a gravel underdrain (approximately 2 ft thick) designed to act as a highly permeable zone to transmit water leaving the system through a network of drainage pipes. A lower-quality limestone was used to ensure the drainage layer remains intact. Drainage pipe (SDR35) was included in this layer and connected to Schedule 40 PVC risers, which transmitted water to the next cell. The drainage layer was then overlain by the organic matter and limestone mixture. All slopes were 2:1 inside and 3:1 outside. Surface area of the first vertical-flow cell (cell 2) was 0.19 acres, and that of the second vertical-flow cell (cell 4) was 0.15 acres.

Each of the vertical-flow cells included horizontal flush lines from the drainage layer designed to be used only during periods of limited maintenance when removal of accumulated solids from the second layer of the vertical-flow cells was deemed to be necessary. The flush lines were set at the approximate elevation of the drainage layer and discharged to the last treatment cell of the system. The flush lines were designed to remain closed during system operation by placement of slide-gate valves downgradient of the vertical-flow cell but upgradient of cell 5.

The surface-flow cells (cells 3 and 5) were excavated to design depth and received no substrate. These cells were designed to reaerate the waters leaving the vertical-flow cells and further oxidatively remove metals from solution. All slopes were 2:1 inside and 3:1 outside. Surface areas of cells 3 and 5 were 0.11 and 0.10 acres, respectively.

2.2 Alkaline Injection Technology

The treatment strategy was designed to create a highly alkaline buffering zone inside the mine by introducing the fluidized-bed combustion (FBC) ash at strategic locations. Conceptually, a buffered region would treat the acidic mine water prior to its discharge and result in lessened surface environment impacts. Once injected into the system, the FBC ash would neutralize existing acid, increase the pH, and impart alkalinity. With elevated pH levels, metal species would precipitate inside the mine as hydroxides and carbonates, among other compounds. The goal was to introduce enough alkaline material to affect the mine system for an extended period of time—what the duration would be was unknown.

3. **PERFORMANCE**

3.1 Passive Treatment Systems

This section contains text taken directly from Porter and Nairn (2008).

Productivity varied among different treatment cells. Nutrient cycling was very rapid to conservative, and macroinvertebrate community diversity, evenness, and trophic structure were relatively high at different sampling locations. The RAPS considered in this study could be defined as an ecosystem in early successional stages based on metrics presented by Odum. Trends in destructive oscillations were observed, and continued discharge of low-oxygenated, high-phosphate water into the later cell will prohibit a trend toward homeostasis. The data collected in this study are not typical of all reducing and alkalinity-producing systems. The presence of more toxic metals and acidic effluents would likely decrease the quality of the communities within the primary treatment cells. Improvements in water quality within the final cells would produce more diverse communities and contribute to more quality ecosystem functions. More extensive research is needed to construct a more defined understanding of ecosystem functions within created ecosystems, specifically RAPS designed to remediate AMD.

3.2 Alkaline Injection Technology

This section contains text taken from Winfrey, Canty, and Nairn (2008).

The ~2500 tons of FBC ash injected into the mine was effective at treating the associated acid mine drainage for 63 months prior to June 2007. Alkaline constituents in the FBC ash altered the mine aquatic chemistry in such a manner that existing acid was neutralized, pH was increased (4.75 to 6.6), alkalinity concentrations increased (<PQL to 227 ppm as CaCO₃), and metals precipitated. As of June 2007, iron, manganese, and aluminum concentrations were approximately 120 ppm, 5.2 ppm and <0.1 ppm, respectively. With the exception of aluminum, pre-injection metals concentrations were being approached (179 ppm, 6.7 ppm, and 3 ppm, respectively). H₂CO₃ was increasing as of June 2007 to nearly preinjection levels, signifying the approaching transition of the final treatment phase of this technology. Also, alkalinity appeared to be gradually increasing as the H₂CO₃ reestablishes equilibrium, while pH was slightly decreasing. Because both of these water quality parameters are changing to a lesser degree than previously observed, it is assumed that treatment Phase 2b was approaching its end. Additional monitoring is needed to evaluate the significance of this transition. Overall, this project has been useful in determining the long-term effectiveness of AIT [alkaline injection technology] as an in situ passive treatment technology for AMD.

In addition, the combination of AIT with other passive treatment technologies is a strategy that has been shown to be effective by this monitoring project. This type of treatment regime could be very useful for abandoned mine reclamation projects that have land available to construct a SAPS [sequential alkaline-producing system].

Parameter	Preinjection (1/95–12/96)	Post-injection (7/97–12/98)
pH	4.4	6.3
Fe (mg/L)	200	80
Al (mg/L)	6	<1
Mn (mg/L)	7	4
SO_4^{2-} (mg/L)	1021	1082
Acidity (mg/L as CaCO ₃ eq.)	439	57
Alkalinity (mg/L as CaCO ₃ eq.)	0	114
Ca (mg/L)	63	289
Mg (mg/L)	40	33

Table 3-1. Median water quality for the Red Oak Mine discharge

Table 3-2. Mean empirically derived contaminant removal rates for passive treatment

systems

	Removal		
	(g per m ² per day)		
Iron in alkaline waters	20		
Manganese in alkaline waters	1		
Acidity in acid waters in surface-flow cells	7		
Acidity in acid waters in vertical-flow cells	30		
Acidity in acid waters in vertical-flow cells	50		
at 40 Gowen demonstration project			

Table 3-3. Calculated and actual design and sizing needs for Red Oak passive treatment
system assuming a hydrologic discharge rate of 20 gpm

Targeted parameter	Concentration (mg/L)	Loading (g/day)	$\begin{array}{c} \text{Design} \\ \text{removal} \\ (\mathbf{g} \cdot \mathbf{m}^{-2} \cdot \mathbf{day}^{-1}) \end{array}$	Calculated area (acres)	Actual area (acres)	Number of cells
Fe	200	21,802	20	0.27	0.21	1
Acidity	450	49,054	30	0.40	0.33	2
Mn (and	7	763	1	0.19	0.22	2
oxygen)						
Totals				0.86	0.76	5

4. COSTS

No information is available.

5. **REGULATORY CHALLENGES**

No regulatory issues were encountered.

6. STAKEHOLDER CHALLENGES

There were no significant public or stakeholder issues associated with the project.

7. OTHER CHALLENGES AND LESSONS LEARNED

Learning to work with private landowners was critical. There was also a need to demonstrate how it would benefit them.

8. **REFERENCES**

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